



ELSEVIER

Contents lists available at ScienceDirect

## Data in Brief

journal homepage: [www.elsevier.com/locate/dib](http://www.elsevier.com/locate/dib)

## Data Article

# Survey dataset on the performance of combined process of coagulation and ceramic membrane for the removal of reactive black19



Ali Jafari<sup>a,b,\*</sup>, Bahram Kamarehi<sup>b</sup>, Akram Ghasemi<sup>b</sup>

<sup>a</sup> Razi Herbal Medicines Research Center, Lorestan University of Medical Sciences, Khorramabad, Iran

<sup>b</sup> Department Of Environmental Health Engineering, Faculty of Health and Nutrition, Lorestan University of medical sciences, Khorramabad, Iran

## ARTICLE INFO

## Article history:

Received 12 May 2018

Received in revised form

20 June 2018

Accepted 27 June 2018

Available online 3 July 2018

## Keywords:

Alum

Ceramic membrane

Chemical coagulants

Ferric chloride

Reactive black19

## ABSTRACT

The aim of data article was to evaluate effectiveness of the combined process of coagulation, flocculation and filtration to remove reactive black 19 from solution aqueous. In this data article, alum and ferric chloride were selected as a coagulant for instability of color before ceramic membrane. All experiments were performed in batch conditions. The results showed that more than half of the ceramic membrane is made of silica. The BET surface area of the ceramic membrane was  $1.877 \text{ m}^2 \text{ g}^{-1}$ . The size of RB19, alum, and ferric chloride was 996.2 nm, 1216 nm, and 86.26 nm, respectively. Also, the zeta potential of RB19, alum, and ferric chloride was 20.7 mV, 1.59 mV, and 34.7 mV, respectively. The findings showed that the best pH to remove the RB 19 by alum and ferric chloride was less than 7. With increasing concentrations of alum and chlorine ferric the removal of RB 19 increased. For RB19 concentration of  $10 \text{ mg l}^{-1}$ , with increasing time from 5 to 15 min, the removal efficiency for alum and ferric were 61–63% and 82–87%, respectively.

© 2018 The Authors. Published by Elsevier Inc. This is an open access article under the CC BY license

(<http://creativecommons.org/licenses/by/4.0/>).

\* Corresponding author at: Razi Herbal Medicines Research Center, Lorestan University of Medical Sciences, Khorramabad, Iran.  
E-mail address: [Jafari\\_a99@yahoo.com](mailto:Jafari_a99@yahoo.com) (A. Jafari).

### Specifications Table

Subject area	Water Chemistry
More specific subject area	Water Treatment
Type of data	Table, figure
How data was acquired	spectrophotometer (UV-UVIS, 594 nm)
Data format	Raw, analyzed,
Experimental Factors	All experiments were performed in batch conditions. The main variables were investigated such as pH, color concentration, coagulation concentration, mixing speed, filtration time. In this data article, the coagulations of alum and ferric chloride were used as coagulant. The final concentration of RB 19 was determined by a spectrophotometer (UV-UVIS, 594 nm)
Experimental features	To determine the structural properties of color, fluke and ceramic membrane by X-ray fluorescence (XRF) spectrometer, Fourier Transform Infrared spectroscopy spectra (FTIR) (Spectrum Two model, PerkinElmer Company), X-ray Diffraction (X' Pert Pro model, Panalytical Company), Energy Dispersive X-ray Spectroscopy, Field Emission Scanning Electron Microscopy (SIGMA VP-500 model, ZEISS Company), and BET surface area and total pore volumes of the samples (BELSORP Mini model, Microtrac Bel Corp) were determined from nitrogen adsorption isotherms at 77 K.
Data source location	Khorramabad city, Lorestan province, west of Iran
Data accessibility	Data are included in this article

### Value of the data

- The hybrid process of coagulation and flocculation was applied to remove reactive black 19 from solution aqueous.
- The data was obtained by sufficient experiments and repetition. The data are useful for developing the same processes and applying for larger scale process.
- This data article shows the capability of the hybrid process of coagulation and flocculation to remove colored effluent.
- The data obtained from this study showed that this combined process could be of interest to environmental authorities.

## 1. Data

In this data article, alum and ferric chloride coagulants as pretreatment step had been suggested to reduce reactive black (RB) color before further treated by ceramic membrane process. The study, RB 19 investigated.

## 2. Experimental design, materials, and methods

All experiments were performed in batch conditions. The main variables were investigated such as pH, color concentration, coagulation concentration, mixing speed, filtration time. In this data article, the coagulations of alum and ferric chloride were used as coagulant. The final concentration of RB 19 was determined by a spectrophotometer (UV-vis, 594 nm). At first for color measurement, calibration curves were drawn ( $Y = 44.603$ ,  $R^2 = 0.9993$ ). Fig. 1 shows used pilot for removal of RB 19. In the Jar-Test, the volume of color solution was 500 ml. Rapid mix speed and contact time were 120 rpm and

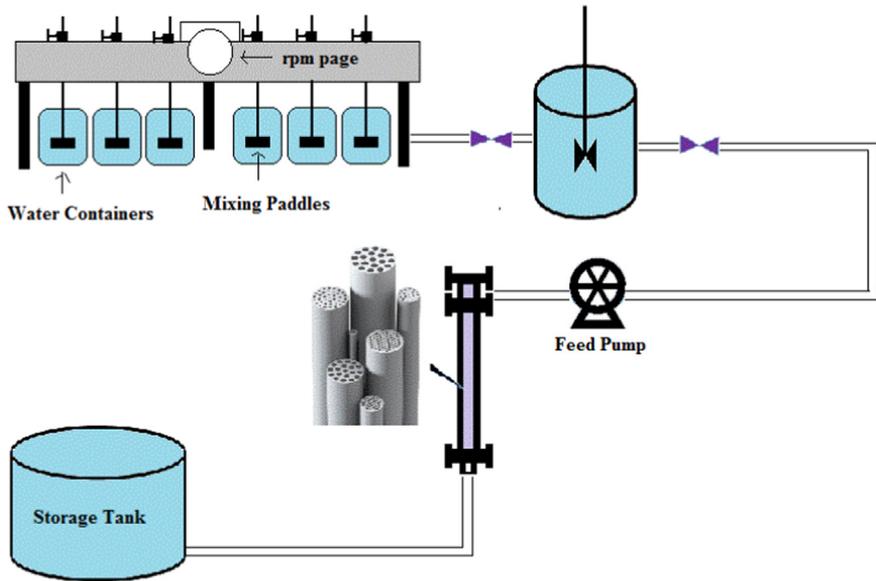


Fig. 1. A view of the used pilot to remove RB 19.

Table 1  
The constituent elements of the ceramic membrane.

Components	%	Components	%
SiO <sub>2</sub>	56.81	P <sub>2</sub> O <sub>5</sub>	0.75
Al <sub>2</sub> O <sub>3</sub>	16.87	SO <sub>3</sub>	Less than 0.1
CaO	16.7	TiO <sub>2</sub>	0.15
MgO	1.63	Na <sub>2</sub> O	0.59
Fe <sub>2</sub> O <sub>3</sub>	2.04	K <sub>2</sub> O	0.74
MnO	Less than 0.1	V <sub>2</sub> O <sub>5</sub>	Less than 0.1

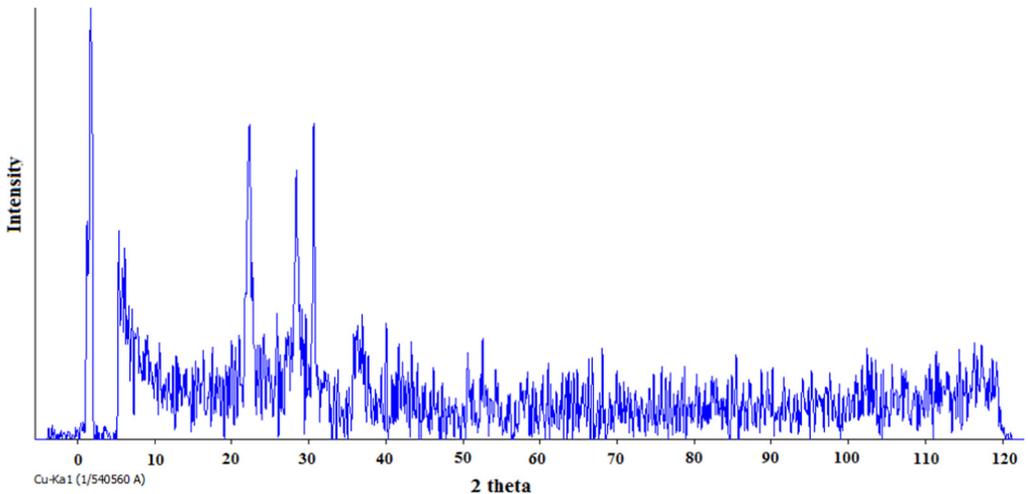
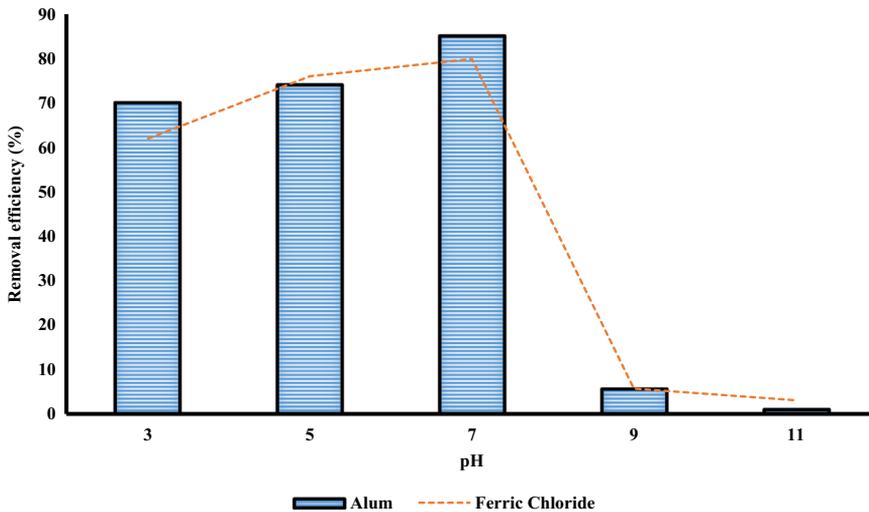


Fig. 2. X-ray diffraction analysis spectra of the ceramic membrane.

**Table 2**

Some properties of ceramic membrane for nitrogen adsorption-desorption experiments at 77 k.

Sample	$SA_{BET}$ ( $m^2 g^{-1}$ )	Total pore volume ( $cm^3 g^{-1}$ )	Mean pore diameter (nm)	Special capacity
Ceramic membrane	1.877	3.8135	128.43	45.085

**Fig. 3.** The effect of pH changes on color removal of RB19 by coagulants ( alum and ferric chloride, and color concentration 30, 30, and 30 mg/l, respectively).

1 min, respectively. Slow mix speed and contact time were 20, 30, 40 rpm and 20 min, respectively. Alum and ferric chloride coagulants were added at various dosages with a fixed color concentration in different pH values.

**Table 1** shows the constituent elements of the ceramic membrane. More than half of the membrane is made of silica ( $SiO_2 \sim 57\%$ ). **Fig. 2** shows X-ray diffraction analysis of ceramic membrane. The BET surface area of the ceramic membrane was  $1.877 m^2 g^{-1}$ . Some properties of the ceramic membrane is shown **Table 2**. To examine for the morphology of ceramic membrane and flock on the filter, scanning electron microscopy was used. The size of RB19, alum, and ferric chloride was 996.2, 1216, and 86.26 nm, respectively. To measure the surface charge density of the particles, zeta potential test was used. The zeta potential of RB19, alum, and ferric chloride was 20.7, 1.59, and 34.7 mV, respectively. To verify the existence of different functional groups present in RB19 and the ceramic membrane. The FTIR analysis was carried out in the wavelengths  $600\text{--}3500 cm^{-1}$ . Functional groups in the ceramic membrane were C–S ( $630\text{--}790 cm^{-1}$ ), C = S ( $1000\text{--}1250 cm^{-1}$ ), C = N ( $1610\text{--}1680 cm^{-1}$ ), C = C ( $2100\text{--}2250 cm^{-1}$ ), C–H ( $3000\text{--}3100 cm^{-1}$ ), and O–H ( $3100\text{--}3650 cm^{-1}$ ). **Fig. 3** shows the performance of two coagulants at different pH values. The findings showed that the best pH to remove the RB 19 by alum as coagulant was less than 7. At pH = 7, the color removal was almost 85%. **Fig. 4** shows the results of removal of colors with different dosage of alum and chlorine ferric coagulants. The results showed that with increasing concentrations of chlorine ferric the removal efficiency of RB19 increased. The highest removal efficiency of color was

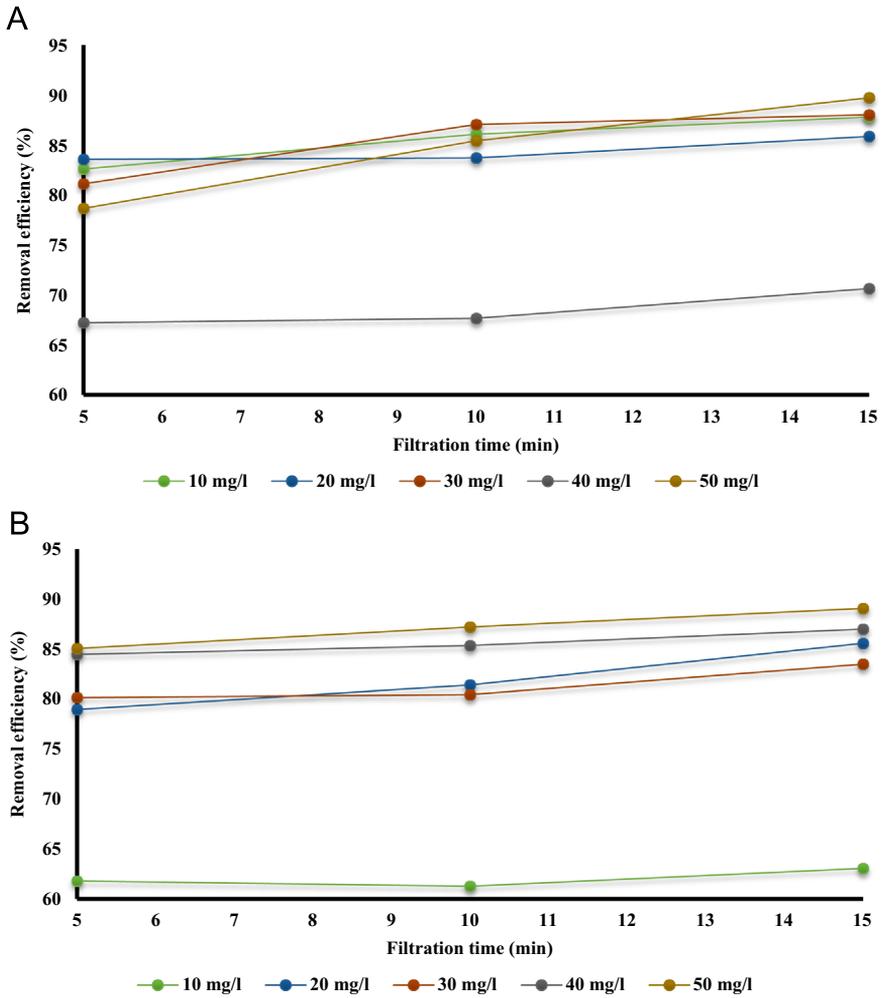


Fig. 4. The effects of coagulant dosage on remove of color A. ferric chloride, B. alum.

**Table 3**  
Changes of combined efficiency in various concentrations of RB19.

Coagulant type	Filtration time (min)	Color concentration (mg/l)				
		10	20	30	40	50
Ferric chloride	5	82.60	83.57	81.12	67.22	78.66
	10	86.10	83.72	87.07	67.66	85.43
	15	87.81	85.88	88.03	70.64	89.74
Alum	5	61.79	78.96	80.15	84.46	85.06
	10	61.27	81.42	80.45	85.36	87.21
	15	63.05	85.58	83.50	86.99	89.07

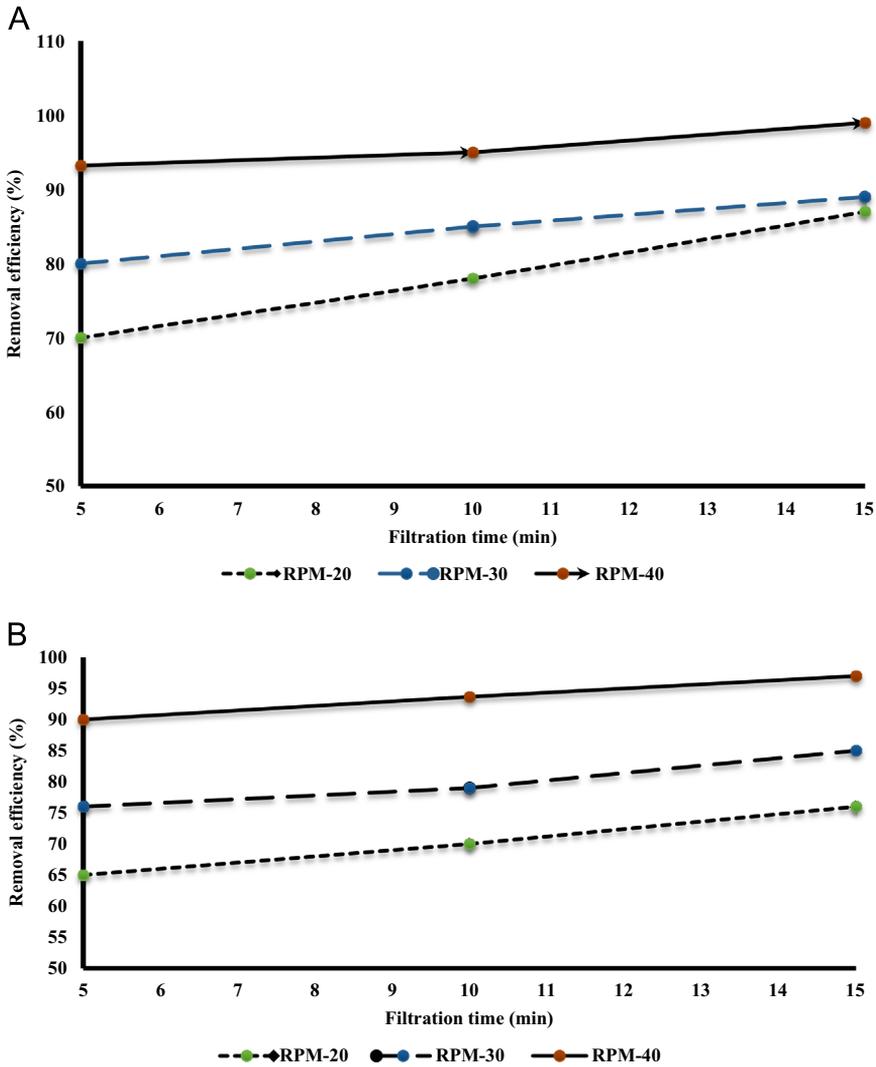


Fig. 5. Changes of combined efficiency in various rpm A. ferric chloride, B. alum.

observed at  $50 \text{ mg l}^{-1}$ . Table 3 shows the changes of removal efficiency with color concentration. With the increasing color concentration in constant dosage, removal efficiency gradually reduced. To ferric coagulant with increasing RB19 concentration from 10 to  $50 \text{ mg l}^{-1}$ , the removal efficiency reduced. Fig. 5 shows the removal of color in with different mixing rates of ferric chlorine and alum coagulant. The results showed that with the increase of slow mixing rate, the color removal increased. Fig. 6 show permeate flux of combined process of coagulation (ferric chloride and alum) and the ceramic filter. The results showed that the permeate flux declines by the time operation [1–18].

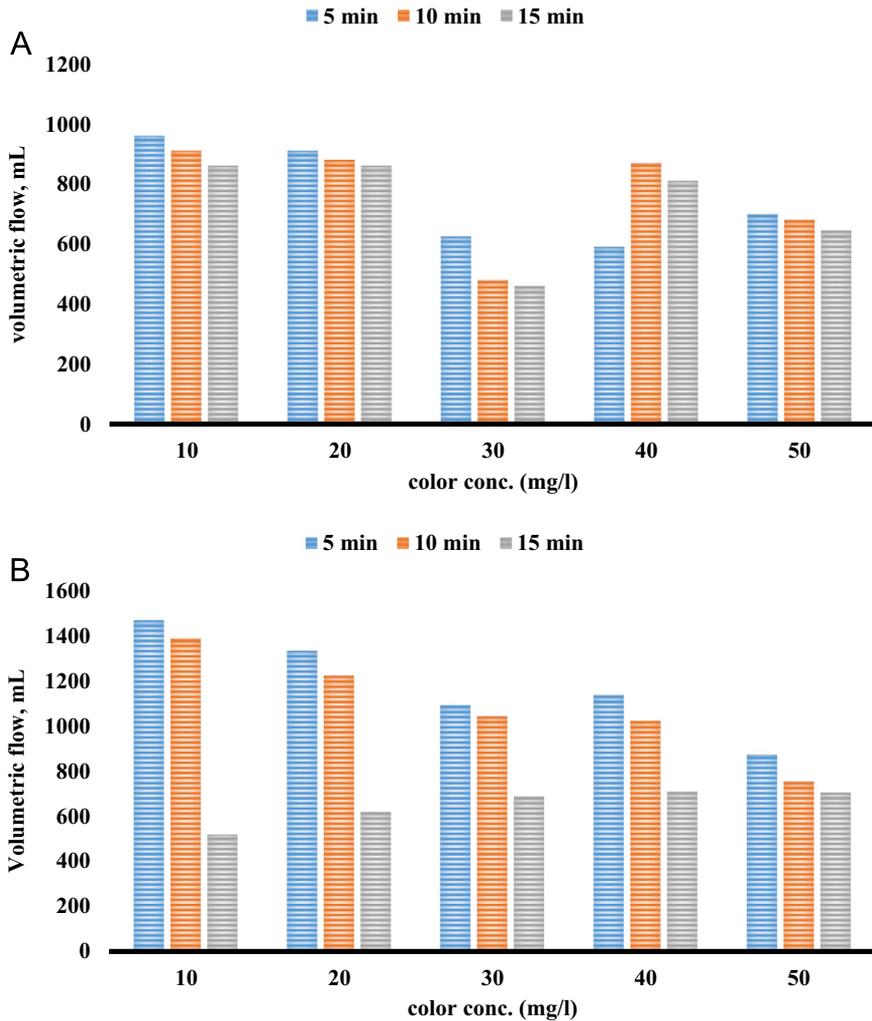


Fig. 6. A. ferric chloride + ceramic filter, B. alum + ceramic filter.

## Acknowledgements

The authors are very appreciate for financial supporting of this research (project no A-10-1412-2) from Lorestan University of Medical Science, Iran.

## Transparency document. Supplementary material

Transparency document associated with this article can be found in the online version at <https://doi.org/10.1016/j.dib.2018.06.114>.

## References

- [1] U.A. Saed, M.H.A. Nahrain, A.A. Atshan, Adsorption of methylene blue dye from aqueous solution using can papyrus, *J. Babylon. Univ./Eng. Sci.* 1 (2014) 218–229.
- [2] T. Phani Madhavi, M. Srimurali, K. Nagendra Prasad, Color removal from industrial waste water using alum, *J. Environ. Res. Dev.* Vol. 8 (04) (2014).
- [3] Z. Derakhshan, M.A. Baghapour, M. Ranjbar, M. Faramarzian, Adsorption of methylene blue dye from aqueous solutions by modified pumice stone: kinetics and equilibrium studies, *Health Scope* 3 (2013) 136–144.
- [4] A.A. Mohammadi, A. Alinejad, B. Kamarehie, S. Javan, A. Ghaderpoury, M. Ahmadpour, M. Ghaderpoori, Metal organic framework Uio-66 for adsorption of methylene blue dye from aqueous solutions, *Int. J. Environ. Sci. Technol.* 14 (2017) 1959–1968.
- [5] H. Hayat, Q. Mahmood, A. Pervez, Z.A. Bhatti, S.A. Baig, Comparative decolorization of dyes in textile wastewater using biological and chemical treatment, *Sep. Purif. Technol.* 154 (2015) 149–153.
- [6] H. Najafi Saleh, M.H. Dehghani, R. Nabizadeh, A.H.M. Mahvi, Y. kamyar, H. Faraji, M. Ghaderpoori, M. Yousefi, A.A. Mohammadi, Data on the acid black 1 dye adsorption from aqueous solutions by low-cost adsorbent-Cerastoderma lamarcki shell collected from the northern coast of Caspian Sea, *Data Brief* 17 (2018) 774–780.
- [7] H.A. Aziz, S. Alias, F. Assari, M.N. Adlan, The use of alum, ferric chloride and ferrous sulphate as coagulants in removing suspended solids, colour and COD from semi-aerobic landfill leachate at controlled pH, *Waste Manag. Res.* 25 (2007) 556–565.
- [8] G.W. Go, E.J. Lee, S. Kang, A. Jang, Combined coagulation/ceramic membrane ultrafiltration system for reclamation of degreasing washing water, *Desalin. Water Treat.* 57 (2016) 7479–7486.
- [9] A. Jafari, A.H. Mahvi, S. Nasser, A. Rashidi, R. Nabizadeh, R. Rezaee, Ultrafiltration of natural organic matter from water by vertically aligned carbon nanotube membrane, *J. Environ. Health Sci. Eng.* 13 (2015) 51.
- [10] A. Jafari, R. Rezaee, S. Nasser, A.H. Mahvi, A. Maleki, M. Safari, B. Shahmoradi, H. Daraei, Application of micellar enhanced ultrafiltration (MEUF) for arsenic (v) removal from aqueous solutions and process optimization, *J. Disper. Sci. Technol.* 18 (2017) 1588–1593.
- [11] M.H. Dehghani, A. Naghizadeh, A. Rashidi, E. Derakhshani, Adsorption of reactive blue 29 dye from aqueous solution by multiwall carbon nanotubes, *Desalin. Water Treat.* 51 (2013) 7655–7662.
- [12] M.H. Dehghani, A. Dehghan, A. Najafpour, Removing Reactive Red 120 and 196 using chitosan/zeolite composite from aqueous solutions: kinetics, isotherms, and process optimization, *J. Ind. Eng. Chem.* 51 (2017) 185–195.
- [13] H. Najafi Saleh, M.H. Dehghani, R. Nabizadeh, A.M. Mahvi, K. Yaghmaeian, H. Faraji, M. Ghaderpoori, M. Yousefi, A. Mohammadi, Data on the acid black 1 dye adsorption from aqueous solutions by low-cost adsorbent-Cerastoderma lamarcki shell collected from the northern coast of Caspian Sea, *Data Brief* 17 (2018) 774–780.
- [14] M.H. Dehghani, P. Mahdavi, Removal of acid 4092 dye from aqueous solution by zinc oxide nanoparticles and ultraviolet, *Desalin. Water Treat.* 54 (2015) 3464–3469.
- [15] M.H. Dehghani, P. Mahdavi, I. Tyagi, S. Agarwal, V.K. Gupta, Investigating the toxicity of acid dyes from textile effluent under UV/ZnO process using *Daphnia magna*, *Desalin. Water Treat.* 68 (2016) 183–189.
- [16] M.H. Dehghani, A.R. Mesdaghinia, S. Nasser, A.H. Mahvi, K. Azam, Application of SCR technology for degradation of reactive yellow dye in aqueous solution, *Water Qual. Res. J. Can.* 43 (2008) 1–10.
- [17] M.H. Dehghani, A. Dehghan, H. Alidadi, M. Dolatabadi, M. Mehrabpour, A. Conventi, Removal of methylene blue dye from aqueous solutions by a new chitosan/zeolite composite from shrimp waste: kinetic and equilibrium study, *Korean J. Chem. Eng.* 6 (2017) 1699–1707.
- [18] M.H. Dehghani, J. Jaafari, A. Alghasi, G. Parkar, Using medium pressure ultraviolet reactor for removing azo dyes in textile wastewater treatment plant, *World Appl. Sci.* 6 (2011) 797–802.